

## MOTIVATION

- Hypersonic vehicles experience aerodynamic heat loads:
  - Cause very high temperatures on their surface
  - Use Thermal Protection System (TPS)
  - Prolonged exposure to high temperature and chemical reactions can cause TPS to fail
- Depending on the heat load
  - Ablative TPS (eg. Stardust)
  - Non-ablative TPS (eg. Space shuttle)
- Surface heating affected by:
  - Catalycity of the TPS material
  - Chemical reaction between the surface material and boundary layer gases → surface recession

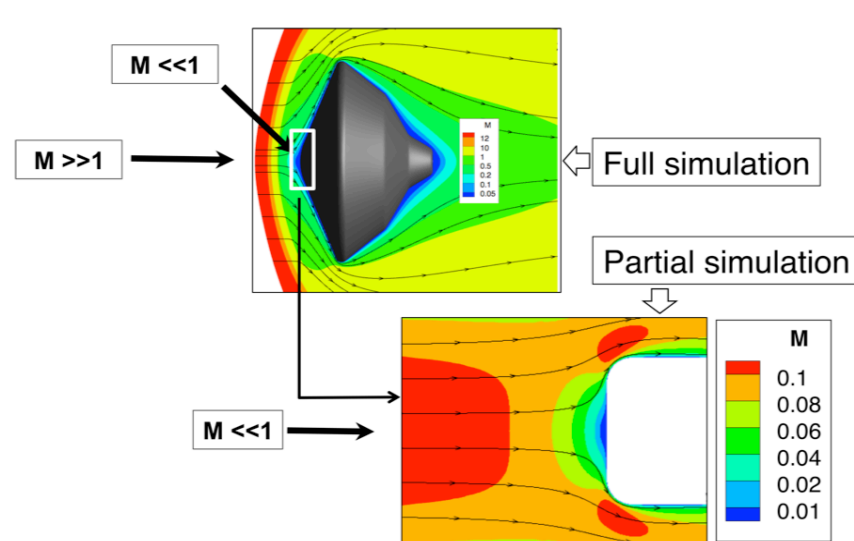
Accurate modeling of these gas-surface interactions is necessary for the prediction of aerothermal heating of the vehicle TPS

## OBJECTIVES

- Investigate surface chemistry models to describe dominant gas-surface interaction processes (e.g. catalysis, nitridation) implemented in a CFD code.
  - current study is an extension to previous studies (AIAA-2012-534, RTO-AVT-199-2012, AIAA-2013-0187)
  - gas-surface interaction model used (surface catalysis and surface participating reactions eg. nitridation, oxidation)
  - Gas considered: Pure Nitrogen
  - physical accuracy of the computational results assessed using experimental data generated in high-enthalpy facility at the University of Vermont (UVM)
  - sensitivity analysis of the free stream chemical composition performed

## FLOW DOMAIN INVESTIGATED

Entry flight environment considered: Post shock subsonic high enthalpy gas flow



## TECHNICAL APPROACH

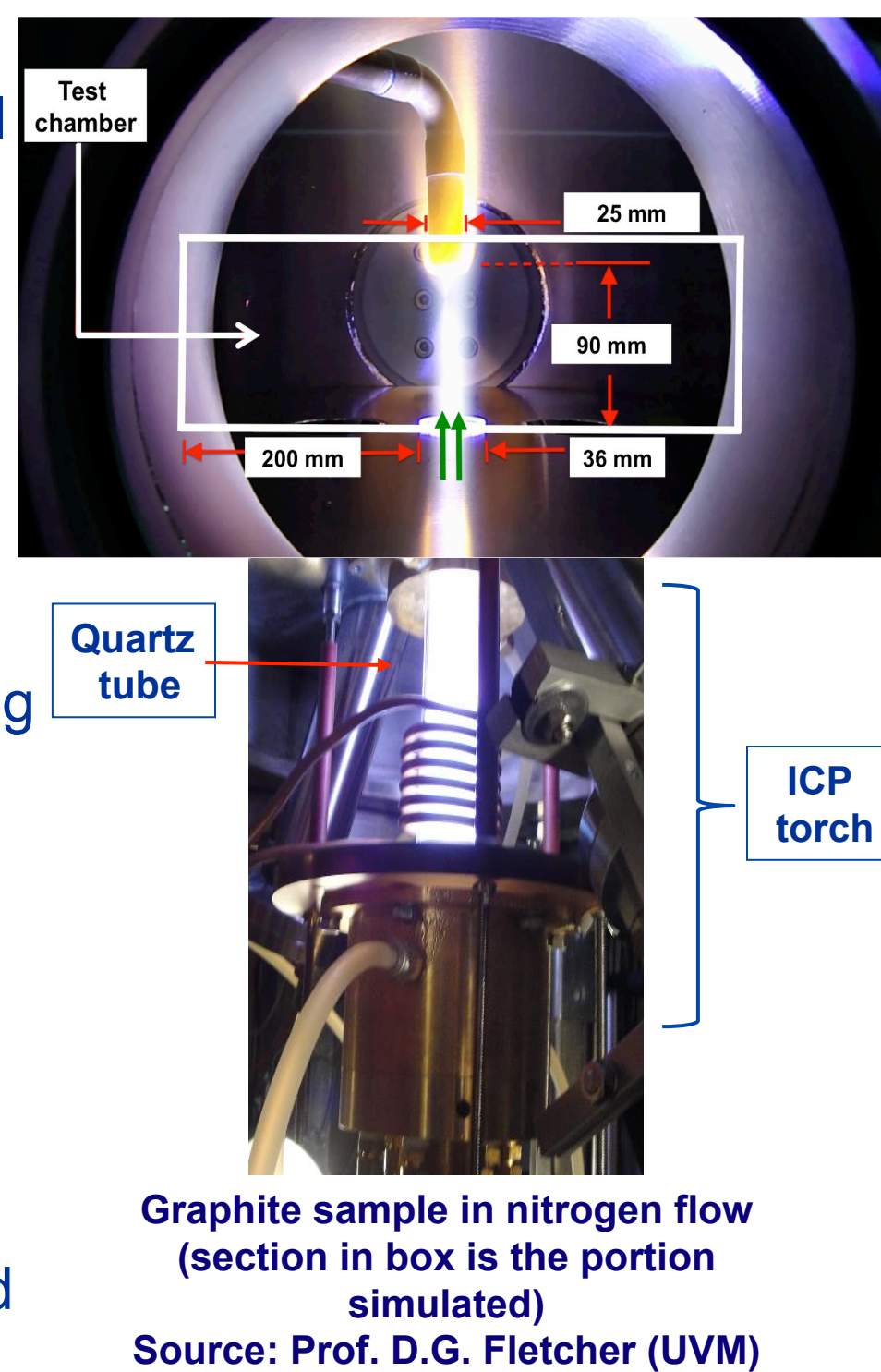
- Computational Tools:** LeMANS: CFD code developed at the University of Michigan (Scalabrin and Boyd: AIAA-2006-3773)
  - solves laminar Navier-Stokes equations
  - can account for thermo-chemical nonequilibrium effects
  - finite volume algorithm with point/line implicit time integration
  - 2D/3D/Axisymmetric simulations on structured/unstructured grids
  - parallelized using domain decomposition

## TECHNICAL APPROACH

- Species boundary conditions**
  - finite rate surface chemistry (FRSC) model (Maclean & Marshall 2011, Alkandry et. al 2012): surface catalysis and surface participating reactions (eg. nitridation, oxidation)
  - Gas-surface interaction processes studied:
    - recombination of N atoms to molecules at the surface due to catalysis
    - carbon nitridation: N atoms react with the surface carbon to form gaseous CN
  - FRSC model used to simulate a constant reaction efficiency  $\gamma$ 
    - $N + (s) \rightarrow N(s)$ : Adsorption ( $E_{ad} = 0$  J/mol)
 
$$N + N(s) \rightarrow N_2 + (s)$$
: Eley-Rideal recombination ( $E_{ER} = 0$  J/mol)
 
$$\gamma = \frac{2S_0\gamma_N}{S_0 + \gamma_N}$$
    - $N + (s) \rightarrow N(s)$ : Adsorption ( $E_{ad} = 0$  J/mol)
 
$$N + N(s) \rightarrow N_2 + (s)$$
: Eley-Rideal recombination ( $E_{ER} = 0$  J/mol)
 
$$C_b + N + (s) \rightarrow CN + (s)$$
: Eley-Rideal recombination ( $E_{ER} = 0$  J/mol)
 
$$\gamma = \frac{2S_0\gamma_N + \gamma_{CN}\gamma_N}{S_0 + \gamma_N}$$

## ASSESSMENT OF COMPUTATIONS

- Assessment of simulations performed using experimental tests at UVM
  - 30 kW Inductively Coupled Plasma (ICP) Torch Facility
- Samples exposed to high enthalpy subsonic gas flows
- Flow quantities measured using two-photon Laser Induced Fluorescence (LIF) technique:
  - Relative N-atom number density
  - Translational temperature
- Surface temperature and sample ablation also quantified



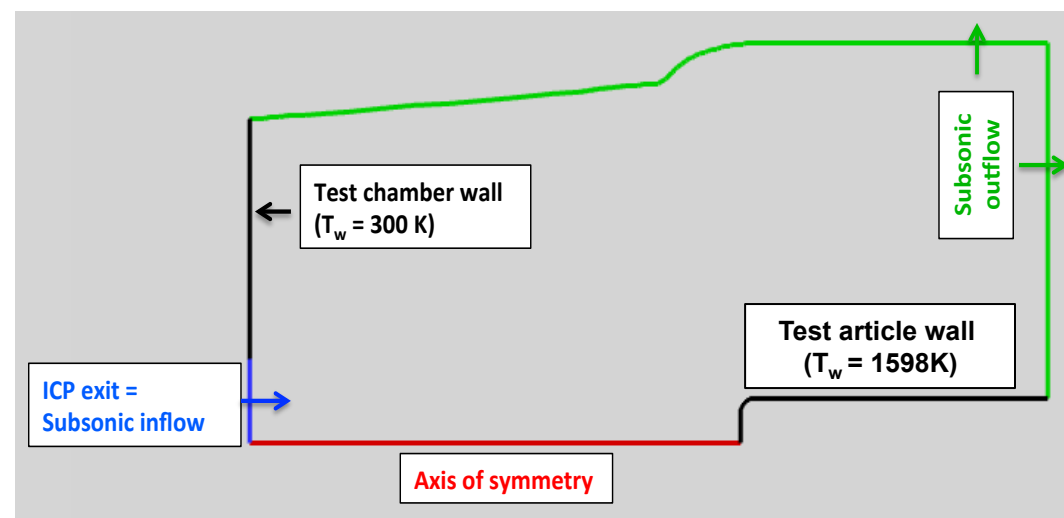
## NUMERICAL SETUP

- Free stream values and wall temperature based on experimental setup

Mass flow rate [kg/s]	$T_\infty$ [K]	$P_\infty$ [kPa]	$T_w$ [K]
$0.82 \times 10^{-3}$	7000	21.3	1598

- Inlet chemical composition calculated using
  - Chemical Equilibrium with Applications (CEA)
  - Power =  $\dot{m}\Delta h$ 

$$\Delta h = \sum_{i=N,N_2} Y_i \int_{298}^T C_{p,i} dT + \sum_{i=N,N_2} Y_i \Delta h_{f,i}^0$$
 Inlet Power  $\approx 13.8$  kW
  - Flow physics model: Thermochemical nonequilibrium
  - Radiative equilibrium
  - Grid generated: Pointwise
    - 22,000 quadrilateral cells

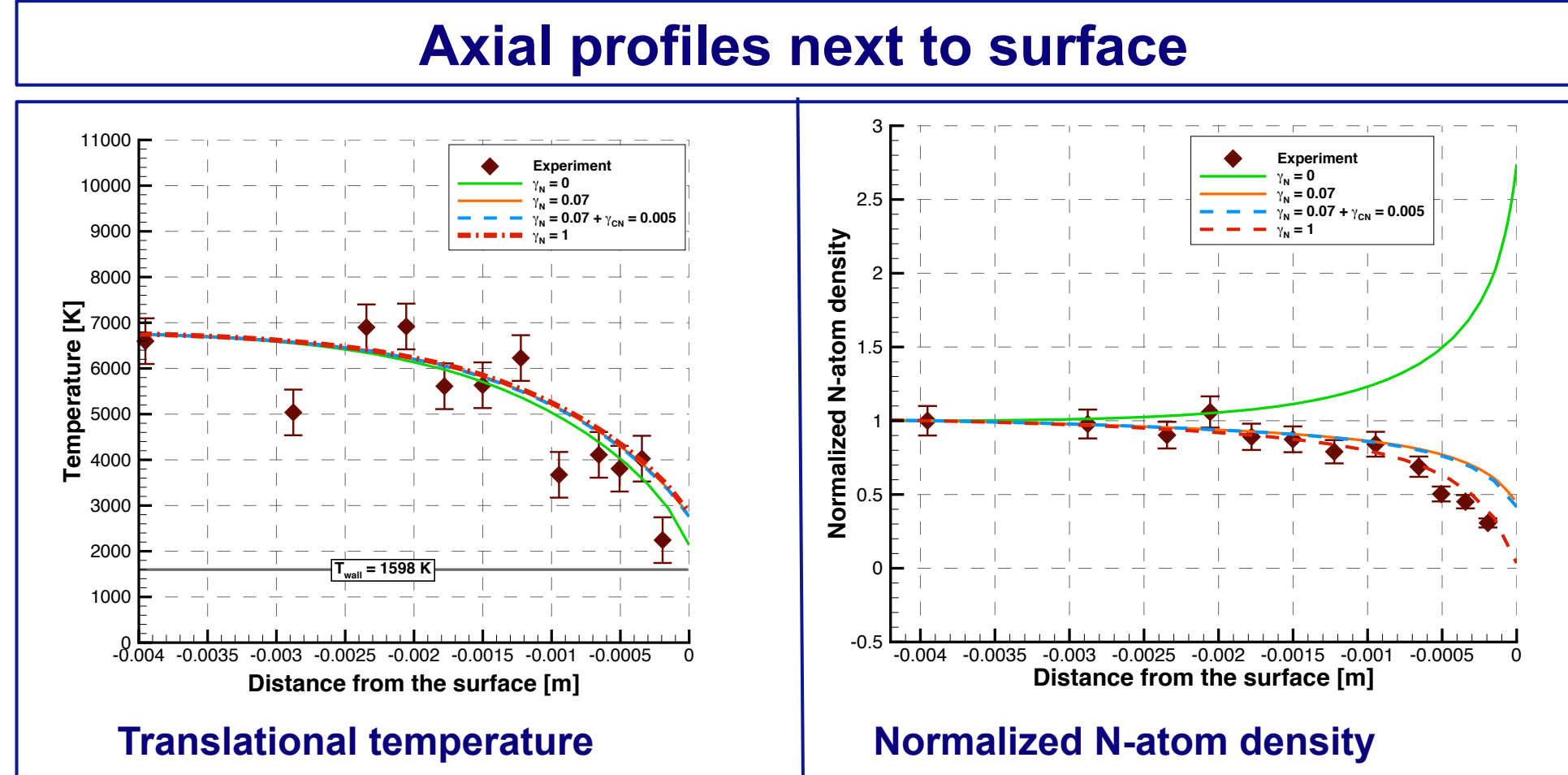


## Acknowledgments

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- Prof. Doug Fletcher and his graduate students, University of Vermont

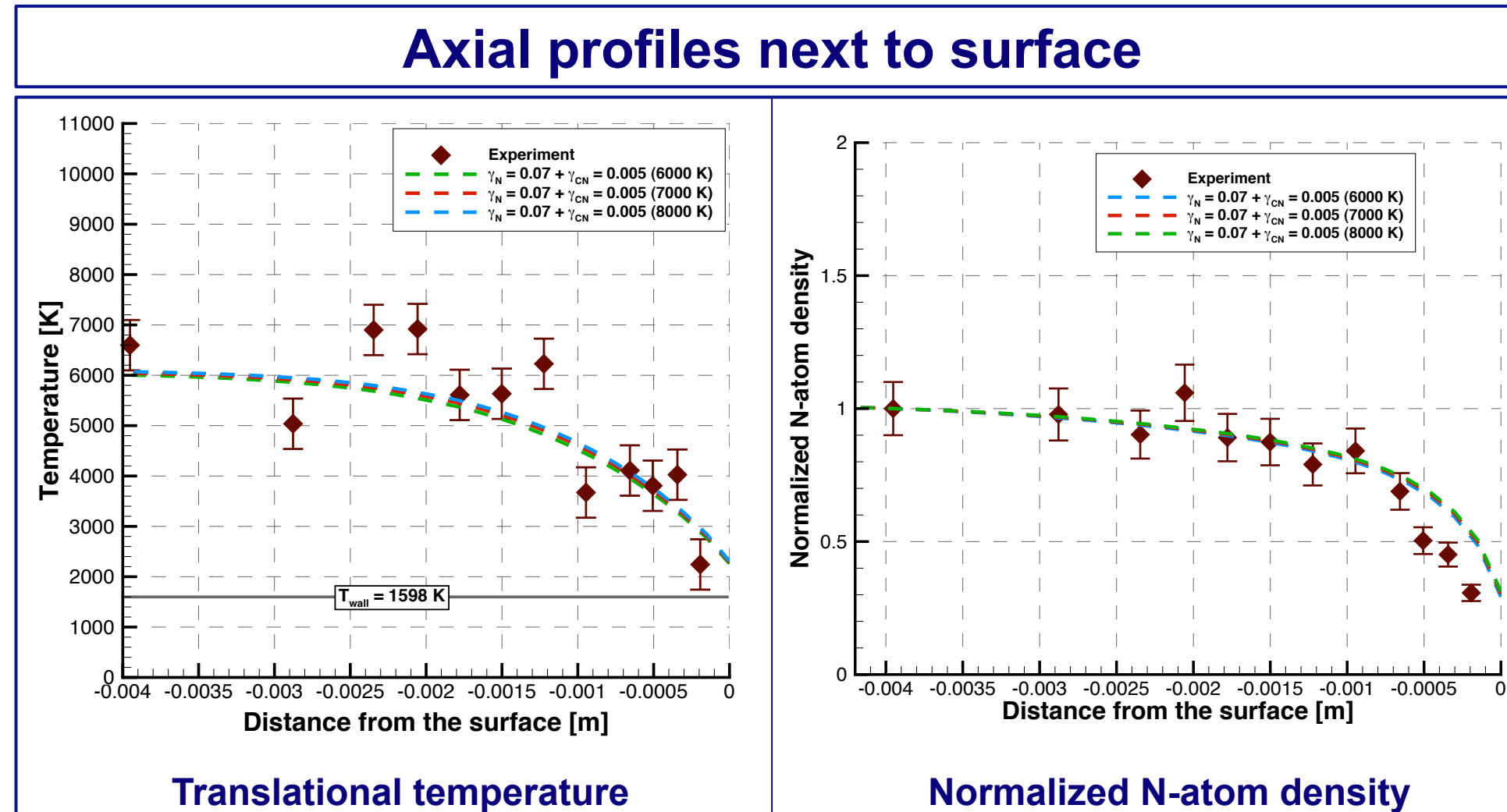
## RESULTS

### Comparison with Experimental Data



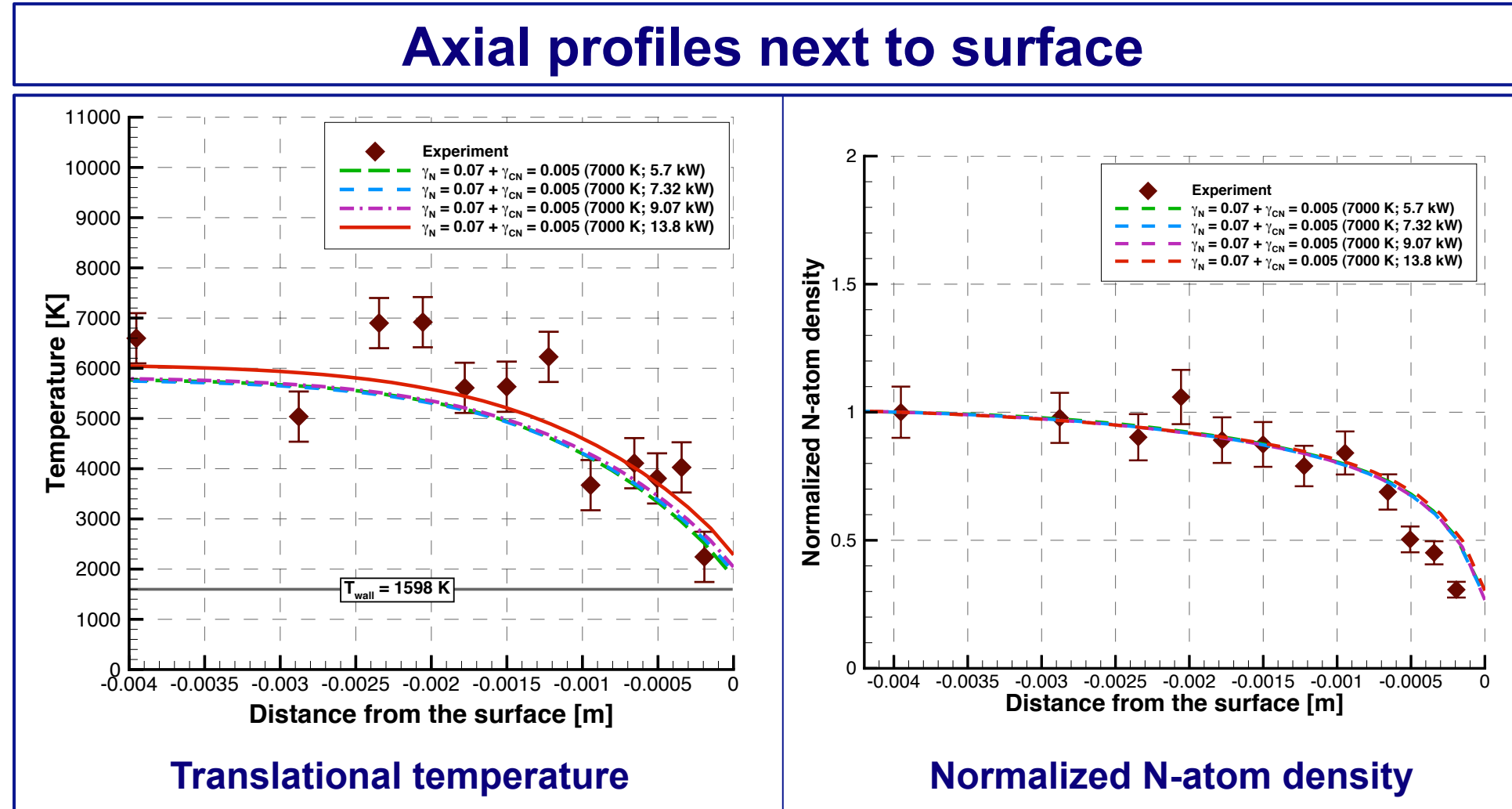
inlet composition	$T_\infty$ [K]	$q_{stag}$ [W/cm <sup>2</sup> ]	$T_{stag}$ [K]	mass loss rate [kg/s]
CEA	7000	270.415	2757.542	2.213
13.8 kW	7000	127.783	2284.063	0.861

### Sensitivity to Inlet Temperature (Power = 13.8 kW)



Power [kW]	$T_\infty$ [K]	$q_{stag}$ [W/cm <sup>2</sup> ]	$T_{stag}$ [K]	mass loss rate [kg/s]
13.8	6000	122.258	2258.888	0.831
13.8	7000	127.783	2284.063	0.861
13.8	8000	133.198	2307.974	0.899

### Sensitivity to Inlet Power



Power [kW]	$X_N$	$T_\infty$ [K]	$q_{stag}$ [W/cm <sup>2</sup> ]	$T_{stag}$ [K]	mass loss rate [kg/s]
5.7	0	7000	51.856	1820.910	0.113
7.3	0.1	7000	65.953	1934.392	0.265
9.1	0.2	7000	81.662	2041.070	0.422
13.8	0.423	7000	127.783	2284.063	0.861
Experiment		$\sim 7000$	40 - 80	$\sim 1600$	0.2 - 0.6

## CONCLUSIONS

- Temperature in the boundary layer not affected by different surface reactions
- Nitrogen atom density decreased when surface chemistry was included
- Carbon mass loss, stagnation temperature and heat flux
  - decreased significantly for chemical composition calculated using inlet power as opposed to the equilibrium composition calculated using CEA
  - not significantly sensitive to inlet temperature
  - significantly sensitive to inlet power